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Signed

Stephen Hordley

Dated

8 July 2003

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GB 0216834.2

By virtue of a direction given under Section 30 of the Patents Act 1977, the application is proceeding in the name of

AEA TECHNOLOGY BATTERY SYSTEMS LIMITED,
329 Harwell,
DIDCOT,
Oxfordshire,
OX11 0QJ,
United Kingdom

Incorporated in the United Kingdom,

[ADP No. 08559585001]



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1. Your reference

15683 TpCm

2. Patent application number

(The Patent Office will fill in this part)

0216834.2

19 JUL 2002

3. Full name, address and postcode of the or of each applicant (underline all surnames)

Accentus plc
329 Harwell
Didcot, Oxfordshire, OX11 0QJ
United Kingdom

Patents ADP number (if you know it)

If the applicant is a corporate body, give country/state of its incorporation

England and Wales

4. Title of the invention

Porous polymeric membrane

5. Name of your agent (if you have one)

Peter Turquand Mansfield

"Address for service" in the United Kingdom to which all correspondence should be sent (including the postcode)

Accentus plc
Patents Department, 329 Harwell
Didcot, Oxfordshire, OX11 0QJ

Patents ADP number (if you know it)

8143497001

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Country

Priority application number
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Date of filing
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7. If this application is divided or otherwise derived from an earlier UK application, give the number and the filing date of the earlier application

Number of earlier application

Date of filing
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8. Is a statement of inventorship and of right to grant of a patent required in support of this request? (Answer 'Yes' if:

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Description	12 ✓
Claim(s)	2 ✓ <i>DMC</i>
Abstract	1 ✓
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Translations of priority documents

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Request for preliminary examination and search (*Patents Form 9/77*)

1 ✓

Request for substantive examination (*Patents Form 10/77*)

Any other documents
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M. J. LOFFING

(on behalf of Accentus plc
by virtue of a Power of Attorney
dated 5th April 2001)

I/We request the grant of a patent on the basis of this application.

Signature

M. J. Loffing

Date

17.07.02

12. Name and daytime telephone number of person to contact in the United Kingdom

01235 432037 Mrs C A Cassidy

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Porous polymeric membrane

The present invention relates to porous polymeric membranes. The invention relates in particular to a process for producing a porous polymeric membrane and to the use of such a membrane in a lithium cell or in a fuel cell.

For many years it has been known to make cells with lithium metal anodes, and cathodes of a material into which lithium ions can be intercalated or inserted. Such cells may use, as electrolyte, a solution of a lithium salt in an organic liquid such as propylene carbonate, and a separator such as filter paper or polypropylene. More recently the use of a solid-state ion-conducting polymer has also been suggested as an electrolyte. For secondary or rechargeable lithium cells, the use of lithium metal anodes is unsatisfactory as problems arise from dendrite growth. The elimination of this problem is now possible by employing a material able to intercalate lithium ions reversibly at very low voltages, such as graphite, leading to so-called "lithium-ion", "rocking-chair", or "swing" lithium rechargeable batteries. These lithium cells operate on the principle that they contain not lithium metal, but lithium ions which are rocked back and forth between two intercalation materials during the charging and discharging parts of the cycle.

A polymer electrolyte has been proposed by Gozdz et al. (US 5,296,318), which comprises a copolymer of 75 to 92% vinylidene fluoride and 8 to 25% of hexafluoropropylene, blended with a lithium salt and a compatible solvent such as ethylene carbonate/propylene carbonate mixture and cast from solution in a low boiling-point solvent such as tetrahydrofuran. It is also possible to make such a solid polymer electrolyte by

first making a porous film of the polymer material, and then immersing the film in the solution of lithium salt in an organic solvent so the electrolyte solution combines with the polymer film, as described in EP 0 730 5 316 A (Elf Atochem). However, with known methods of making porous membranes, it is difficult to achieve micropores of a substantially uniform size and to control the porosity of the resulting film.

10 Fuel cells use a porous membrane to separate the anode and the cathode. The membrane is typically a multilayered assembly and may include, for example, a porous membrane and one or more diffusion layers. Improved membranes are needed to improve the uniform 15 delivery of gas to the fuel cell plate.

The present invention provides a process for producing a porous polymeric membrane which process comprises:

20

a) preparing a solution comprising a polymer which comprises vinylidene fluoride in a solvent /non-solvent mixture by dispersing the polymer in the non-solvent prior to addition of the solvent;

25

b) holding the solution at an elevated temperature until the polymer is completely solvated;

30

c) casting the solution to form a thin layer; and

d) drying the thin layer to form a membrane.

The polymer typically comprises primarily vinylidene fluoride. Thus the polymer may be a homopolymer such as 35 polyvinylidene fluoride (PVdF), or a copolymer of vinylidene fluoride with, for example hexafluoro-

propylene, or a terpolymer. Typically preferred grades of polymer are PVdF homopolymer Solvay Solef 1015 or 6020, copolymers Solvay Solef 20615 or 20815 or Atochem 2801 and terpolymers comprising vinylidene fluoride,
5 hexafluoropropylene and chlorotrifluoroethylene as described in WO 02/11230.

Further components may also be present in the solution for example, viscosity modifiers such as
10 carboxymethylcellulose and surface tension modifiers such as oxalic or maleic acid.

The polymer is mixed with the non-solvent to form a slurry and then the solvent is added to form a
15 homogeneous solution. Typically a slurry of polymer and non-solvent is formed and heated to about 60°C, preferably in a non-metallic container (for example of glass, or of a plastic such as polypropylene) with stirring, and then the solvent is added rapidly (for
20 example at about 1 litre in 5 seconds).

If the polymer is mixed with the solvent first, and the non-solvent then added to the solution, this generates a microgel, so the solution is unstable and
25 does not give reproducible membranes.

The non-solvent is a liquid which does not dissolve the polymer when used alone. The non-solvent should not only dissolve in the solvent, but it should be miscible
30 with the solvent in substantially all proportions. Typically, the boiling point of the non-solvent is higher than that of the solvent, preferably 20°C higher, more preferably 40°C higher or more. Examples of the non-solvents include alcohols containing 6 to 20 carbon atoms
35 such as, octanol, decanol and dodecanol, and mixtures thereof, preferably decanol, dodecanol and mixtures

thereof. Particularly preferred non-solvents are a 50:50 mixture of dodecanol and decanol or dodecanol alone.

5 The solvent is a liquid which can dissolve or swell the polymer. The solvent may be chosen from for example ketones, ethers, N,N-dimethylformamide (DMF), N,N-dimethylacetamide (DMA), N,N-diethylacetamide, N-methyl-2-pyrrolidone (NMP), hexamethylphosphoramide, tetramethylurea and dimethyl sulfoxide (DMSO) or a
10 mixture thereof. DMF and NMP are preferred solvents. More preferably NMP is the solvent.

The ratio of non-solvent to solvent in the solution can be varied. Typically the proportion of non-solvent in
15 the solvent/non-solvent mixture is 2 to 30 wt %, preferably 5 to 15 wt %, more preferably 7 to 10 wt%.

The amount of polymer in the solution is generally from 3 to 30 wt %, preferably from 5 to 20 wt %, more
20 preferably from 8 to 15 wt %.

Solvation of the polymer takes place at an elevated temperature. An elevated temperature is a temperature above room temperature (which is taken to be 20°C). The
25 temperature chosen is specific to the polymer and solvent/non-solvent combination that is used and the amount of time over which solvation takes place. Typically the elevated temperature is at least 40°C, more typically at least 50°C for example 55°C. A lower
30 temperature may be used if solvation takes place over an even longer period of time.

Typically solvation takes place over several days. The solvation process continues until the polymer(s) are
35 completely solvated. The exact solvation time required varies depending on the solvent/non-solvent mixture, the

choice of polymer or polymers and the temperature used. Typically solvation takes place over from 4 to 14 days, preferably 5 to 10 days and most preferably 5 to 7 days. For example, PVdF (Solvay Solef 6020/1001) in N-methyl-2-pyrrolidone and a 50:50 mixture of decanol and dodecanol typically solvates completely in from 5 to 14 days, typically 10 days depending on the ratio of non-solvent to solvent in the solution. Gel formation during the solvation process is so slow as to be negligible. Solvation also occurs without the formation of a microgel.

Once the polymer is fully solvated, the solution is stable at room temperature for several weeks. Thus, the viscosity of the solution does not change over time, the colour of the solution remains constant and there is no separation of the solvent or non-solvent from the solution. Furthermore the solution forms reproducible membranes with consistent properties, when cast. Therefore it is not necessary to cast the solution into a film immediately.

The solution is typically cast onto a non-porous substrate such as aluminium foil or Mylar film. The aluminium foil is typically about 20 μm thick whereas the Mylar film is typically about 100 μm thick. The solution can also be cast onto an anode or cathode if the anode or cathode is made of a material that is not too porous.

When casting the solution, the solution is typically cast as a thin layer less than 0.5 mm thick, preferably less than 0.3 mm thick, on the substrate.

The film is formed by drying in at least two successive drying zones in a drying machine; the film is not contacted with any liquids. Preferably the drying

machine has three or four drying zones, most preferably four drying zones. Different temperatures are maintained in each of the zones and the temperatures increase from zone to zone in the direction of the film transfer.

- 5 Typical temperature values in the drying zones when using a knife-over-roll continuous method for producing a membrane on a moving web are as follows:

10	first zone	from 50°C to 120°C
	second zone	from 80°C to 150°C.

Typical temperature pairings could be, for example, 65°C in the first zone and 100°C in the second zone, or 95°C in the first zone and 120°C in the second zone. If the
15 machine has three or four drying zones then the temperature change from zone to zone can be more gradual. For example, where the machine has four drying zones, the zones can be set at 65°C, 75°C, 95°C and 110°C in order.

20 The speed of the moving web typically ranges from 0.2 to 5.0 m/min. The speed of the web varies depending on the length of the drying zone and the number of zones. The more zones the machine has, the faster the web can be run without adverse effects on the properties of the
25 membrane.

The solution is dried to form a membrane in the presence of a gas. In one embodiment the gas is dry gas, for example dry air. For example, air with a dewpoint of
30 less than -20°C, for example from -35°C to -37°C may be used. However, the gas need not be anhydrous. The gas may also be humid air, for example air supplied at ambient conditions of 34% relative humidity at 16°C. However if
35 air humidity varies, the membrane's permeability will
also vary.

The porosity of the resulting porous polymeric membrane can be controlled by varying the ratio of non-solvent to solvent, the ratio of polymer to solvent/non-solvent, the temperatures of the first and the second drying zones and the speed of the moving web.

The porosity of the membrane produced can be measured on a Gurley machine. This gives an indication of the relative porosity of different films measured using this machine. The machine measures the time taken in seconds for 100 cm³ of air to pass through one square inch (6.45 cm²) of the membrane at a small standard pressure difference (1.215 kPa). This results in a reading known as a Gurley number or Gurley value. This can also be expressed as having the units Gurley seconds. Commercial films are available which give Gurley numbers (Gurley seconds) of from 400 to 600. Films with a Gurley number of <60 tend to exhibit shorting when used in a battery. However, they may be suitable for use in fuel cells. The films with a Gurley number of from 50 to 200, more preferably 60 to 100, are preferred in the context of the present invention. As Gurley numbers increase the porosity of the membrane decreases indicating that it is harder to pass air through the membrane. This could be due to the membrane having smaller pores or fewer larger pores depending on the distribution of the pores.

Films as thin as 5 µm can be made according to the present invention. Thus, the films have a thickness of at least 5 µm, preferably 10 to 30 µm, more preferably 15 to 25 µm, most preferably 17 to 22 µm.

One advantage of the present invention is that thin films can be made which have adequate strength to be used in a battery. The thin films also do not suffer from

shorting.

In a second aspect the present invention provides a membrane comprising a polymer comprising vinylidene fluoride with a thickness of from 5 to 30 μm and a Gurley number of from 5 to 300 (Gurley seconds). The membranes preferably have a Gurley number of from 50 to 200, more preferably from 60 to 100, most preferably from 70 to 90. Such membranes have not hitherto been available.

10

The present invention also provides the use of a membrane of the present invention or of a membrane produced according to the present invention as a separator in a battery. The membrane is suitable for use in a range of different types of battery, for example, nickel-cadmium, nickel metal hydride, lithium ion and lithium polymer batteries. The controllable porosity and thickness of the membrane as well as the high strength of these membranes makes them particularly advantageous for this use.

20

The present invention also provides the use of a membrane of the present invention or a membrane produced according to the process of the present invention in a fuel cell. The present invention also provides a laminate comprising a membrane of the present invention and the use such a laminate in a fuel cell.

25

The present invention is now described in greater detail by way of example.

30

Examples

The Gurley numbers given for the membranes described in these examples were obtained on an Automatic Densometer model 4340 produced by Gurley Instruments of

35

514 Fulton Street, Troy, New York, USA.

Example 1

5 100 g PVdF (Solef 6020) having an intrinsic
viscosity of 0.210 l/g (DMF, 25°C) was dispersed in 70 g
of octanol. The slurry was stirred and 900 g of DMF was
added. The mixture was stirred for 1 day at 55°C and
maintained at 55°C for 6 further days until complete
10 solvation was achieved.

The solution was cast onto a polyester web moving at
0.5 m/minute using a knife-over-roll coating system. The
blade gap was set to 0.32 mm and the drying zone
15 temperatures were 65°C for zone 1 and 100°C for zone 2.
This resulted in a finished microporous film with a
thickness of 17 µm and an air permeability of 32 Gurley
seconds.

20 Increasing the drying temperatures to 80°C for zone
1 and 105°C for zone 2 produced a film with a thickness
of 17 µm and an air permeability of 85 Gurley seconds.

25 Further increasing the drying temperatures to 95°C
for zone 1 and 110°C for zone 2 produced a film with a
thickness of 17 µm and an air permeability of 93 Gurley
seconds.

Example 2

30 100 g of PVdF (Solef 6020) having an intrinsic
viscosity of 0.210 l/g (DMF, 25°C) was dispersed in 80 g
of decanol. The slurry was stirred and 900 g of NMP was
added. The mixture was stirred and heated until complete
35 solvation was achieved as described in Example 1.

The solution was cast onto a polyester web moving at 0.5 m/minute using a knife-over-roll coating system. The blade gap was set to 0.32 mm. The drying zone temperatures and film properties are set out in Table 1 below.

Table 1

	Example 2.1	Example 2.2
Drying zone temp. Zone 1 (°C)	95	110
Drying zone temp Zone 2 (°C)	110	130
Film thickness (µm)	14	16
Air permeability (Gurley secs)	12	40

10

Example 3

100 g of PVdF (Solef 6020) having an intrinsic viscosity of 0.210 l/g (DMF, 25°C) was dispersed in 70 g of a 1:1 mixture (by weight) of decanol and dodecanol. The slurry was stirred and 900 g of NMP was added. The mixture was stirred for 1 day at 55°C and maintained at 55°C for 10 further days until complete solvation was achieved.

20

The solution was cast onto a polyester web moving at 0.5 m/minute using a knife-over-roll coating system. The blade gap was set to 0.32 mm. The drying zone temperatures and film properties are set out in Table 2 below.

25

Table 2

	Example 3.1	Example 3.2
Drying zone temp. Zone 1 (°C)	75	110
Drying zone temp. Zone 2 (°C)	110	130
Film Thickness (µm)	13	18
Air Permeability (Gurley secs)	70	180

5 Example 4

100 g of PVdF (Solef 6020) having an intrinsic viscosity of 0.210 l/g (DMF, 25°C) was dispersed in 100 g of a 1:1 mixture (by weight) of decanol and dodecanol.
10 The slurry was stirred and 900 g of NMP was added. The mixture was stirred and heated until complete solvation was achieved as described in Example 3.

The solution was cast onto a polyester web moving at
15 0.5 m/minute using a knife-over-roll coating system. The blade gap was set to 0.32 mm. The drying zone temperatures and film properties are set out in Table 3 below.

Table 3

	Example 4.1	Example 4.2
Drying zone temp. Zone 1 (°C)	75	110
Drying zone temp. Zone 2 (°C)	110	130
Film Thickness (µm)	22	24
Air Permeability (Gurley secs)	9	55

It will be appreciated from the above Examples that
5 the porosity becomes less (i.e. the Gurley number
increases) if the dryer is at a higher temperature, and
if the proportion of non-solvent is less. Film quality
is generally improved if the difference in boiling point
between the non-solvent and the solvent is greater than
10 25°C.

Claims

1. A process for producing a porous polymeric membrane which process comprises:
 - 5 a) preparing a solution comprising a polymer which comprises vinylidene fluoride in a solvent/non-solvent mixture by dispersing the polymer in the non-solvent prior to addition of the solvent;
 - 10 b) holding the solution at an elevated temperature until the polymer is completely solvated;
 - c) casting the solution to form a thin layer; and
 - 15 d) drying the thin layer to form a membrane.
2. Process according to claim 1 wherein the solution comprises polyvinylidene fluoride (PVdF).
- 20 3. Process according to claim 1 or 2 wherein the solvent is N,N-dimethylformamide (DMF), N,N-dimethylacetamide (DMA) or N-methyl-2-pyrrolidone (NMP).
- 25 4. Process according to any of claims 1 to 3 wherein the non-solvent is octanol, decanol, dodecanol or a mixture thereof.
5. Process according to any of claims 1 to 4 wherein
30 the solution is solvated for up to 14 days.
6. A membrane produced by the process of any of claims 1 to 5.
- 35 7. A membrane comprising a polymer comprising vinylidene fluoride with a thickness of from 5 to 30 μm and a Gurley

number of from 5 to 300.

8. A membrane according to claim 7 wherein the membrane has a Gurley number of from 50 to 200.

5

9. A membrane according to claim 8 wherein the membrane has a Gurley number of from 60 to 100.

10. A laminate comprising a membrane produced according to the process of any of claims 1 to 5 or a membrane according to any of claims 7 to 9.

11. Use of a membrane produced according to the process of any of claims 1 to 5 or a membrane according to any of claims 7 to 9 in a battery.

12. Use of a membrane produced according to the process of any of claims 1 to 5 or a membrane according to any of claims 7 to 9 in a fuel cell.

20

13. Use of a laminate according to claim 10 in a fuel cell.

14. A membrane substantially as described herein with reference to any one of the Examples.

15683 TpCm

P.T. Mansfield
Chartered Patent Agent
Agent for the Applicants

30

Abstract

Porous polymeric membrane

5 A process for producing a porous polymeric structure
which process comprises preparing a solution comprising a
polymer which comprises vinylidene fluoride in a
solvent/non-solvent mixture; holding the solution at an
elevated temperature until the polymer is completely
10 solvated; casting the solution to form a thin layer; and
drying the thin layer to form a membrane. The polymer is
dispersed in the non-solvent before addition of the
solvent, when preparing the solution, to prevent microgel
formation. The prolonged solvation at elevated
15 temperature provides a stable solution, and enables
membranes of controlled porosity to be formed.

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